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On void fraction and flow fragmentation in two-phase gas-liquid free-surface flows



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1. Introduction

The interactions between high-velocity liquids and the atmosphere may lead to strong gas-liquid mixing and complex multiphase flow interactions [4,8,15]. Relevant applications encompass chemical, nuclear, civil, mechanical and environmental engineering situations. The resulting gas-liquid mixture consists of both gas bubbles surrounded by liquid and droplets surrounded by gas, inclusive of foam, spray and complex gas-liquid structures [10,12,17]. The entrainment of gas packets can be localised, as at the impingement of plunging jets [1,9], or continuous along the gas-liquid interface, e.g. on a spillway chute [2,19] (Fig. 1).

In high-velocity free-surface flows, the gas volume fraction ranges from very small values to unity in the atmosphere. Traditional monophase flow measurement technique are affected by the dilute phase and the gas-liquid interfaces. The most robust method is the phase-detection needle probe [3,5,6,13]. The probe tip is designed to pierce the gas-liquid interfaces and the resulting signal is a pseudo-square-wave signal, as illustrated in Fig. 2A. Fig. 2A show instantaneous void fraction data (blue curve) and post-processed signal using a single threshold technique. In Fig. 2A, each signal drop corresponds to a liquid-to-gas interface, while the following signal rise is a gas-to-liquid interface detection. Over the sampling period, the signal averaging gives the time-averaged void fraction

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ABSTRACT

In free-surface flows, the interactions between high-velocity liquid and atmosphere may lead to strong gas-liquid mixing and complex multiphase flow interactions. In this study, the void fraction power spectrum density (PSD) is used to provide an alternative view of the air-water flow composition. The high frequency range of the PSD curve reflects contributions of small chord times, while the low frequency range contains contributions of both small and large chord times. Likewise, the interactions between the smallest bubbles contribute approximately uniformly to the entire frequency range of the spectrum, while any interaction involving large bubbles/drops will be modulated by $1/f^2$. It is shown that the void fraction spectra are a powerful tool in providing an alternative view of the air-water flow composition.

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and the rate of liquid-to-gas interface detections yields the bubble frequency.

In the present study, the processing of phase-detection probe signal is re-visited. It is shown that the instantaneous signal of a single-sensor probe includes informations in terms of both phase bulk and gas-liquid composition. These properties are developed, and physical observations are discussed.

2. Basic considerations on gas-liquid structure

Considering a streamtube through a phase-detection needle sensor, the flow may be reduced to a streamwise distribution of small discrete gas and liquid elements, comprised of the smallest discrete air-water particles of length scale λ_{aw} , as shown in Fig. 2B. λ_{aw} is selected such that the probability of one element being gas or liquid becomes independent of the adjacent elements. Focusing on each pair of adjacent gas-liquid elements defined as 1 and 2 respectively, a gas-liquid interface is detected when element 1 is gas and element 2 is liquid, or element 1 is liquid and element 2 is gas.

For a segment of gas-liquid signal, in which the number of small discrete gas and liquid elements is N_a and N_w respectively, the probability of one element being gas (Pr(a)) or liquid (Pr(w)) is respectively:

$$Pr(a) = \frac{N_a}{N_a + N_w} = C$$
(1)

$$Pr(w) = \frac{N_w}{N_a + N_w} = 1 - C$$
⁽²⁾



(A) Laboratory experiment - Q = 0.084 m³/s, Re = 3.4×10^5 , h = 0.10 m, $\theta = 45^{\circ}$



(B) Hinze dam prototype spillway on 7 May 2015 - Q = 21 m³/s, Re = 6.7×10^6 , h = 1.2 m, θ = 51.3°

Fig. 1. Interfacial aeration along a stepped spillway chute.

where C is the time-averaged void fraction. Eqs. (1) and (2) assume implicitly no-slip between the gas and liquid interfaces, a quasi-steady streamtube velocity, and a significantly large number of gas-liquid elements, all of these being reasonable assumptions in high-velocity free-surface flows, e.g. as in Fig. 1. The total number of gas-to-liquid interfaces equals that of liquid-to-gas interfaces. Considering the former, the average number of gas bubbles detected by the probe sensor per second equals the bubble frequency F:

$$F = NPr(a)Pr(w) = \frac{U_{aw}}{\lambda_{aw}}C(1 - C)$$
(3)

where N is the average number of elemental interfaces detected by the probe sensor per second and U_{aw} the fluid velocity. Eq. (3) predicts a quasi-parabolic relationship between bubble frequency and mean void fraction across the gas-liquid column, thus a pseudo linear relation between the root mean square of the instantaneous void fraction and the bubble frequency. An extended solution yields a relationship between bubble frequency and interfacial turbulence intensity [18].

A few studies [7,11] discussed the use of spectral analysis performed on the phase-detection probe signal output. The power spectral density (PSD) of a binary void fraction signal is defined as the square of the discrete Fourier transform (DFT) coefficients:

$$S_{c} = E(FFT(c')FFT^{*}(c'))$$
(4)

where S_c is the void fraction PSD, FFT is the fast Fourier transform, * denotes the complex conjugate, c' is the instantaneous void fraction deviation from the mean value, and E is the expectation operator.

The shape of the void fraction PSD reflects contributions from all individual bubble/droplet sizes. The bandwidth of a bubble's contribution to the PSD is inversely proportional to its physical size. Namely, a small bubble/droplet contributes approximately equally to all frequencies, while a large bubble/drop contributes predominantly to the low frequency range. A theoretical analysis shows that the void fraction power decays as $1/f^2$ at the end of the spectrum, where f is the frequency. Thus, a characteristic size of the smallest gas bubbles may be defined as $1/f_c$, where f_c is a characteristic frequency beyond which the PSD slope visually follows $1/f^2$.

3. Void fraction spectra

The analysis of a single-sensor phase detection probe $(\emptyset = 0.25 \text{ mm})$ was conducted in the stepped chute, and for the flow conditions, shown in Fig. 1A. The water discharge was Q = 0.071 m³/s, the Reynolds number was $Re = 2.8 \times 10^5$, the vertical cavity height was h = 0.10 m, and the chute slope was $q = 45^{\circ}$. The phase-detection probe was sampled at 5 kHz for 180 s, as preliminary tests showed that a relatively long sampling duration was important as part of the proposed technique. Fig. 3A shows the distributions of time-averaged void fraction and bubble frequency at step edge 12. The void fraction PSD was estimated using Welch's [16] method. Each void fraction signal was first divided into 29 sub-segments, each of 1/15th the total length of the signal, taken with a 50% overlap; each segment was then multiplied by a Hann window to reduce boundary effects before calculating discrete Fourier transform (DFT) was calculated. The final result was taken as the average over the 29 total modified PSDs. The void fraction signals were thresholded and detrended prior to computation. Fig. 3B shows the void fraction spectrum data. In Fig. 3B, let us note the variety of shapes displayed by the PSD curves at different elevations. By the Wiener-Khinchin theorem, $S_c(f)$ and $R_{xx,c}(\tau)$ form a Fourier transform pair. Therefore the area under each curve is proportional to the variance of the signal, equalling C(1-C) [14]. Thus, in the first approximation, the integral $\int S_c df$ is proportional to the bubble frequency F. More details are presented in the Supplementary material Appendix I.



(A) Phase-detection probe signal output in a stepped chute - $Q = 0.084 \text{ m}^3/\text{s}$, $Re = 3.4 \times 10^5$, h = 0.10 m, $\theta = 45^\circ$, mean void fraction: C = 0.68



(B) Streamwise distribution of discrete two-phase elements assuming $\lambda_{aw} = \lambda_a = \lambda_w r$, following Toombes and Chanson (2008)



The expected shape of a void fraction spectrum may be analysed theoretically by treating a binarised void fraction signal as a linear superposition of pulse trains, each characterised by a unique duration corresponding to the chord time of the bubbles under consideration. The expected shape of the void fraction spectra should follow:

/ ...

$$E(S_{c}(f)) = \frac{1}{\pi^{2}f^{2}N} \left(\sum_{i=1}^{N_{p}} N_{bi} \sin^{2}(\pi f\tau_{ci}) + \frac{8}{\pi^{2}} \sum_{i=1}^{N_{p}-1} \sum_{j=i+1}^{N_{p}} N_{i}N_{j} \sin(\pi f\tau_{ci}) \sin(\pi f\tau_{cj}) \right)$$
(5)

where N_b is the total number of bubbles in a pulse train, N_p is the total number of pulse trains, N is the total length of the signal, f is the frequency (horizontal axis of PSD data), and τ_c is a unique bubble chord time for each pulse train. The complete derivation is shown in Supplementary material Appendix I. Eq. (5) holds for all $f \neq 0$, and the $S_c(0)$ term is simply zero if the data is detrended before calculation (i.e. zero mean). In Eq. (5), the shape of a void fraction spectrum is the sum of contributions from each unique bubble chord time as well as interactions between every pair of chord times. A detailed interpretation of the properties of Eq. (5) is developed in Supplementary material Appendix I.

In summary, the dependence of $E(S_c(f))$ on a single chord time τ_{ci} reflects the fact that a narrow (wide) band signal in the frequency domain have a wide (narrow) counterpart in the time domain, namely:

(a) for $\tau_{ci} \approx 0$ (very small bubbles/droplets), the contribution is approximately equal to all frequency components in the PSD; and

(b) for $\tau_{ci} > 0$ (very large bubbles/droplets), the contribution is dominantly to the low frequency range in the PSD and decays with $1/f^2$ in the high frequency range;

Consequently, the high frequency range of the PSD curve reflects contributions of small chord times, whereas the low frequency range contains contributions of both small and large chord times. Likewise, the interactions between the smallest bubbles contribute approximately uniformly to the entire frequency range of the spectrum, while any interaction involving large bubbles/droplets will be modulated by $1/f^2$.

3.1. Discussion

Gonzalez [11] hinted that the void fraction spectrum may be divided into two zones about a characteristic frequency f_c : i.e. $f < f_c$ and $f > f_c$, each representing the total energy in the signal due to the largest and smallest length scales, where f_c may be identified from a change in slope in the spectra. In the present study, Eq. (5) suggests that both small and large length scales contributed to the low frequency range of the spectrum. Rather, a characteristic frequency f_c may be defined as where the spectrum visually follows $1/f^2$. In such case, U_{aw}/f_c could be loosely interpreted as the smallest air bubble length scale in the flow.

In reference to Fig. 3B, a preponderance of small chord times is observed next to the step edge (red and black curves) and large chord times are dominant in the spray zone ($y/Y_{90} > 1$). The former case reflects the large rate-of-strain next to the step edge, where a significant number of small bubbles are generated. The latter case implies a flow primarily consisting of water globules of large chord sizes.



(A) Vertical distributions of time-averaged void fraction C and bubble frequency F



(B) Void fraction spectra in the stepped chute flow

Fig. 3. Void fraction distribution and spectra in a stepped chute flow - Q=0.084 m³/s, $Re = 3.4 \times 10^5$, h = 0.10 m, $\theta = 45^{\circ}$, step edge 12, $Y_{90} = 0.0518$ m, $V_{90} = 4.10$ m/s, $F_{max} = 272$ Hz.

4. Conclusion and future work

The present study indicates that the void fraction PSD may be used to provide an alternative view of the air-water flow composition, including a new way to interpret the information contained in the PSD of a phase function signal. Information such as the bubble count rate and characteristic air-water chord size can be inferred. The void fraction distribution is implied by combining the bubble count rate and air-water chord size information: e.g. small bubble count rate and large chord size imply low void fraction.

The dependence of the void fraction spectrum $E(S_i(f))$ on a single chord time τ_{ci} reflects the fact that a narrow (wide) band signal in the frequency domain have a wide (narrow) counterpart in the time domain. The high frequency range of the PSD curve reflects contributions of small chord times, while the low frequency range contains contributions of both small and large chord times. Likewise, the interactions between the smallest bubbles contribute approximately uniformly to the entire frequency range of the spectrum, while any interaction involving large bubbles/drops will be modulated by $1/f^2$. Importantly, the void fraction spectra are a powerful tool in providing an alternative view of the air-water flow composition. This method has the advantage of aggregating a number of qualitative information in one glance, including the bubble count rate and air-water chord sizes. The void fraction might be inferred by combining the bubble count rate and air-water chord size information (e.g. small bubble count rate and large chord size imply low void fraction).

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Supplementary materials

Supplementary material associated with this article can be found, in the online version, at doi:10.1016/j.mechrescom.2019.01. 001.

References

- N.J. Bertola, H. Wang, H. Chanson, Air bubble entrainment, breakup and interplay in vertical plunging jets, J. Fluid. Eng. 140 (9) (2018) 13 ASME Paper 091301, doi:10.1115/1.4039715.
- [2] P. Cain, I.R. Wood, Measurements of self-aerated flow on a spillway, J. Hyd. Div. 107 (HY11) (1981) 1425-1444 ASCE.
- [3] A. Cartellier, J.L. Achard, Local phase detection probes in fluid/fluid two-phase flows, Rev. Sci. Instrum. 62 (2) (1991) 279–303.
- [4] H. Chanson, in: Air Bubble Entrainment in Free-Surface Turbulent Shear Flows, Academic Press, London, UK, 1997, p. 401.
- [5] H. Chanson, Air-water flow measurements with intrusive phase-detection probes. can we improve their interpretation ? J. Hydraul. Eng. 128 (3) (2002) 252–255 ASCE, doi:10.1061/(ASCE)0733-9429(2002)128:3(252).
- [6] H. Chanson, Phase-detection measurements in free-surface turbulent shear flows, J. Geophys. Eng. 13 (2) (2016) S74–S87, doi:10.1088/1742-2132/13/2/S74.
- [7] H. Chanson, C.A. Gonzalez, Interactions between free-surface, free-stream turbulence and cavity recirculation in open channel flows: measurements and turbulence manipulation, in: Y. Matsumoto, K. Hishida, A. Tomiyama, K. Mishima, S. Hosokawa (Eds.), Proceedings 5th International Conference on Multiphase Flow, Yokohama, Japan, 2004, p. 14. Paper 104.
- [8] C. Crowe, M. Sommerfield, Y. Tsuji, in: Multiphase Flows with Droplets and Particles, CRC Press, Boca Raton, USA, 1998, p. 471.
- [9] D.A. Ervine, E.J. McKeogh, E.M. Elsawy, Effect of turbulence intensity on the rate of air entrainment by plunging water jets, *Proc. Instn. Civ. Engrs* Part 2 (June) (1980) 425–445.
- [10] S. Felder, H. Chanson, Air-water flow characteristics in high-velocity freesurface flows with 50% void fraction, *Int. J. Multiphase Flow* 85 (2016) 186–195, doi:10.1016/j.ijmultiphaseflow.2016.06.004.
- [11] C.A. Gonzalez, An Experimental Study of Free-Surface Aeration on Embankment Stepped Chutes *Ph.D. thesis*, Department of Civil Engineering, The University of Queensland, Brisbane, Australia, 2005.
- [12] J.W. Hoyt, J.J. Taylor, Turbulence structure in a water jet discharging in air, Phys. Fluid. 20 (10) (1977) S253-S257 Pt. II, Oct.
- [13] O.C. Jones, J.M. Delhaye, Transient and statistical measurement techniques for two-phase flows: a critical review, Int. J. Multiphase Flow 3 (1976) 89–116.
- [14] Y. Mirai, Y. Oishi, Y. Takeda, F. Yamamoto, Turbulent shear stress profiles in a bubbly channel flow assessed by particle tracking velocimetry, *Exp. Fluid.* 41 (2006) 343–352.

- [15] N.S.L. Rao, H.E. Kobus, Characteristics of self-aerated free-surface flows, Water and Waste Water/Current Research and Practice, 10, Eric Schmidt Verlag, Berlin, Germany, 1971.
- [16] P. Welch, The use of fast fourier transform for the estimation of power spectra: a method based on time averaging over short, modified periodograms, *IEEE Trans. Audio Electroacoust.* 15 (2) (1967) 70–73, doi:10.1109/TAU.1967.1161901.
 [17] I.R. Wood, Air entrainment in free-surface flows, in: IAHR Hydraulic Structures
- [17] I.R. Wood, Air entrainment in free-surface flows, in: IAHR Hydraulic Structures Design Manual No. 4, Hydraulic Design Considerations, Balkema Publ., Rotterdam, The Netherlands, 1991, p. 149.
- [18] G. Zhang, H. Chanson, Interactions between Free-surface Aeration and Total Pressure on a Stepped Chute, *Exp. Therm. Fluid Sci.* 74 (2016) 368–381, doi:10.1016/j.expthermflusci.2015.12.011.
- [19] G. Zhang, H. Chanson, Self-aeration in the rapidly- and gradually-varying flow regions of steep smooth and stepped spillways, *Environ. Fluid Mechan.* 17 (1) (2017) 27-46, doi:10.1007/s10652-015-9442-z.

<u>On Void Fraction and Flow Fragmentation in Two-Phase Gas-Liquid Free-Surface Flows.</u> <u>Appendix I - Spectral properties of a binary void fraction signal</u>

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For a void fraction signal (Fig. 2) consisting of N samples at equal intervals Δt and assuming that the underlying process is wide-sense stationary, its power spectral density (PSD) may be estimated as:

$$S(k) = \frac{1}{N} \left| f_{c}(n) e^{-2\pi i \frac{k}{N} n} \right|^{2}$$
 for integers $k = [0, 1, ..., N/2]$ (I.1)

where $f_c(n)$ is the void fraction sample at index n, i is the imaginary unit such that $i^2 = -1$, and the absolute valued term is the discrete-time Fourier Transform (DFT) of the void fraction record $f_c(n)$. This is known as the periodogram estimate of the true PSD of the underlying random process. While Equation (I.1) is simple to compute, the variance of the periodogram does not tend to zero as N tends to infinity and it is therefore an inconsistent estimator of the true PSD (Oppenheim and Schafer 2010). Welch (1967) proposed that an improved estimate could be obtained by dividing the data into overlapping segments, calculating a modified periodogram for each, and averaging over the segments. Suppose that a record consists of possibly overlapping segments $f_c(n)$ each of size N_i, a modified periodogram for each segment is estimated as:

$$S_{i}(k) = \frac{1}{\sum_{n=1}^{N_{i}} W^{2}(n)} \left| \sum_{n=0}^{N_{i}-1} f_{ci}(n) W(n) e^{-2\pi i \frac{k}{N}n} \right|^{2}$$
 for integers $k = [0, 1, ..., N/2]$ (I.2)

where W(n) is an arbitrary window function. The PSD estimate is then the average over K such periodograms covering the length of the record:

$$S(k) = \frac{1}{K} \sum_{i=1}^{K} S_i(k)$$
(I.3)

Figure 3 shows the distribution of PSDs in a stepped chute (flow conditions listed in figure caption). The results were obtained using the Welch's method with a Hann window:

$$W(n) = \sin^2\left(\frac{\pi n}{N-1}\right)$$
(I.4)

where N is width of the window. The modified periodograms (Eq. (I.2)) were computed for subsamples of $1/15^{th}$ of the total data length with a 50% overlap arbitrarily selected. The resulting PSD estimates were smoothed over every 50 points by delinearising the data, low pass filtering, and reinserting the trend following Press et al. (1986). Note that the void fraction signals were binarised (gas: $f_c(n)=1$; liquid: $f_c(n)=0$) using a single threshold technique and the data mean subtracted before computation.

In Figure 3, the PSD curve at a given elevation is characterised by a distinctive trend and area under the curve. By the Wiener-Khinchin theorem, the area under each curve is proportional to the variance of the signal. Since the variance of a binary void fraction signal equals C(1-C) with C the time-averaged void fraction (Murai et al. 2006), the area under each curve is approximately

proportional to the bubble count rate.

The trend of the PSD curves may be examined by first considering an idealised binary void fraction signal sketched in Figure I-1. The void fraction signal may be regarded as a linear superposition of void fraction pulse trains [f_{c1} , f_{c2} , ..., f_{cN}], each consisting pulses of a unique duration [τ_{c1} , τ_{c2} , ..., τ_{cN}]. Under these settings each pulse on the ith pulse train is activated for a uniform duration τ_{ci} , and T_d^{ij} denotes the time delay of the jth pulse on the ith pulse train measured from the centre of the pulse to the origin. The forward Fourier transform of the jth pulse on the ith pulse train is:

$$FT_{ij}(f) = \int_{T_d^{ij} - \tau_{ci}/2}^{T_d^{ij} + \tau_{ci}/2} e^{-2\pi i f t} dt = e^{-2\pi i f T_d^{ij}} \frac{\sin(\pi f \tau_{ci})}{\pi f}$$
(I.5)

$$fr_{ci}$$



By the linearity property, it follows that the Fourier transform of the ith pulse train is:

$$FT_{i}(f) = \sum_{j=1}^{N_{i}} e^{-2\pi i f T_{d}^{ij}} \frac{\sin(\pi f \tau_{ci})}{\pi f} = A_{i} e^{i\varphi_{ci}} \frac{\sin(\pi f \tau_{ci})}{\pi f}$$
(I.6)

where N_i is the total number of pulses in the ith train, A_i is a characteristic amplitude, and ϕ_{ci} is a characteristic phase such that:

$$\begin{split} \left| A_{i} \right|^{2} &= \left(\sum_{j=1}^{N_{i}} \cos(2\pi f T_{d}^{ij}) \right)^{2} + \left(\sum_{j=1}^{N_{i}} \sin(2\pi f T_{d}^{ij}) \right)^{2} \\ &= N_{i} + 2 \sum_{j=1}^{N_{i}-1} \sum_{k=j+1}^{N_{i}} \left(\cos(2\pi f T_{d}^{ij}) \cos(2\pi f T_{d}^{ik}) + \sin(2\pi f T_{d}^{ij}) \sin(2\pi f T_{d}^{ik}) \right) \end{split}$$
(I.7)
$$\phi_{ci} &= a \tan 2 \left(\frac{\sum_{j=1}^{N_{i}} \sin\left(-2\pi f T_{d}^{ij}\right)}{\sum_{j=1}^{N_{i}} \cos\left(-2\pi f T_{d}^{ij}\right)} \right)$$
(I.8)

where atan2 yields the argument of $e^{i\varphi_{ci}}$ between $-\pi$ and π . The Fourier transform of the entire void fraction signal consisting K pulse trains is:

$$FT(f) = \sum_{i=1}^{K} A_i e^{i\varphi_i} \frac{\sin(\pi f\tau_{ci})}{\pi f}$$
(I.9)

By definition, the periodogram of the void fraction signal is calculated as:

$$\begin{split} S(f) &= \frac{1}{N} \left| FT(f) \right|^2 = \frac{1}{N} FT(f) FT^*(f) \\ &= \frac{1}{\pi^2 f^2 N} \sum_{i=1}^K A_i e^{i\varphi_{ci}} \sin(\pi f\tau_{ci}) \sum_{j=1}^K A_j e^{-i\varphi_{cj}} \sin(\pi f\tau_{cj}) \\ &= \frac{1}{\pi^2 f^2 N} \sum_{i=1}^K \sum_{j=1}^K A_i A_j e^{i(\varphi_{ci} - \varphi_{cj})} \sin(\pi f\tau_{ci}) \sin(\pi f\tau_{cj}) \\ &= \frac{1}{\pi^2 f^2 N} \left(\sum_{i=1}^K A_i^2 \sin^2(\pi f\tau_{ci}) + 2 \sum_{i=1}^{K-1} \sum_{j=i+1}^K A_i A_j \sin(\pi f\tau_{ci}) \sin(\pi f\tau_{cj}) \cos(\varphi_i - \varphi_j) \right) \end{split}$$
(I.10)

where N is the total number of points in the void fraction record and * denotes the complex conjugate. In Equation (I.7), if T_d^{ij} and T_d^{ik} are mutually independent and that the principle values of $2\pi f T_d^{ij}$ and $2\pi f T_d^{ik}$ are uniformed distributed over $[-\pi, \pi]$ for all $f \neq 0$ then:

$$E\left(\sum_{j=1}^{N_{i}-1}\sum_{k=j+1}^{N_{i}}\left(\cos(2\pi fT_{d}^{ij})\cos(2\pi fT_{d}^{ik})+\sin(2\pi fT_{d}^{ij})\sin(2\pi fT_{d}^{ik})\right)\right)=0$$
(I.11)

where E is the expectation operator, and herein we assume ensemble average equals time average (i.e. ergodicity). Using Equation (I.11) and taking the expectation of Equation (I.10) yields:

$$E(S(f)) = \frac{\left(\sum_{i=1}^{K} N_{i} \sin^{2}(\pi f \tau_{ci}) + 2\sum_{i=1}^{K-1} \sum_{j=i+1}^{K} N_{i} N_{j} \sin(\pi f \tau_{ci}) \sin(\pi f \tau_{cj}) E(\cos(\varphi_{i} - \varphi_{j}))\right)}{\pi^{2} f^{2} N}$$
(I.12)

The second expectation in the bracket is less obvious. Consider the bracketed term in Equation (I.8) and assuming that the principle values of $2\pi f T_d^{ij}$ are uniformed distributed over $[-\pi, \pi]$, it follows that the distributions of $\sin(-2\pi f T_d^{ij})$ and $\cos(-2\pi f T_d^{ij})$ are identical and symmetrical about zero. By the central limit theorem (Gnedenko and Kolmogorov 1949), the distributions of the sums of trigonometric terms each tends to a Gaussian in the limit of large N_i, and because the numerator and denominator are exactly correlated the two resulting Gaussian distributions have identical means and variances. Therefore the distribution of the bracketed term is the ratio between two identical Gaussians distributions, which assumes the shape of a standard Cauchy distribution (Papoulis and Pillai 2002):

$$CDF_{\chi}(X) = \frac{1}{\pi} \tan^{-1}(X) + \frac{1}{2}$$
 (I.13)

where $\text{CDF}_{\chi}(X)$ is the cumulative distribution function of the standard Cauchy distribution, where X denotes the bracketed term in Equation (I.8). To find the probability density function of the random variable $\Gamma = \tan^{-1}(X)$, we first note that $Pr(\Gamma \leq \gamma) = Pr(\tan(\Gamma) \leq \tan(\gamma)) = Pr(X \leq \tan(\gamma))$ because $\tan^{-1}(X)$ is a monotonically increasing function of X. Therefore the CDF of Γ is:

$$CDF_{\Gamma}(\gamma) = \frac{\gamma}{\pi} + \frac{1}{2}$$
(I.14)

By differentiating with respect to γ , the left hand side of Equation (I.8) is found to be uniformly distributed between $[-\pi/2, \pi/2]$. Since φ_i and φ_j are independent, the PDF of $Z = (\varphi_i - \varphi_j)$ is obtained directly by convoluting the distributions of φ_i and $(-\varphi_j)$:

$$PDF_{Z}(\zeta) = \int_{-\infty}^{\infty} PDF_{\Gamma}(\gamma) PDF_{-\Gamma}(\zeta - \gamma) d\gamma$$
 (I.15)

The solution is a triangular distribution with width 2π and height $1/\pi$ centred at the origin:

$$PDF_{Z}(\zeta) = \begin{cases} \frac{1}{\pi} + \frac{\zeta}{\pi^{2}} & -\pi \leq \zeta < 0\\ \frac{1}{\pi} - \frac{\zeta}{\pi^{2}} & 0 \leq \zeta < \pi \end{cases}$$
(I.16)

The last expected value in Equation (I.12) may now be evaluated from definition:

$$E(\cos(\zeta)) = \int_{-\pi}^{0} \cos(\zeta) \left(\frac{1}{\pi} + \frac{\zeta}{\pi^{2}}\right) d\zeta + \int_{0}^{\pi} \cos(\zeta) \left(\frac{1}{\pi} - \frac{\zeta}{\pi^{2}}\right) d\zeta = \frac{4}{\pi^{2}}$$
(I.17)

Finally, the expected value of the void fraction PSD is obtained by substituting Equation (I.17) into (I.12):

$$E(S(f)) = \frac{1}{\pi^2 f^2 N} \left(\sum_{i=1}^{K} N_i \sin^2(\pi f \tau_{ci}) + \frac{8}{\pi^2} \sum_{i=1}^{K-1} \sum_{j=i+1}^{K} N_i N_j \sin(\pi f \tau_{ci}) \sin(\pi f \tau_{cj}) \right)$$
(I.18)

which shall hold for all $f \neq 0$. The S(0) term corresponds to the mean of the data and will simply be zero if the data is detrended before calculation.

To understand Equation (I.18), we first consider the shape of the PSD including only the contributions from individual chord times (i.e. the interactions between chord times are neglected):

$$E(S_{i}(f)) = \frac{N_{bi}}{N} \left(\frac{\sin(\pi f \tau_{ci})}{\pi f}\right)^{2}$$
(I.19)

Hence the spectral shape for one chord time depends critically on the behaviour of the function $h(\pi f \tau_{ci}) = \sin(\pi f \tau_{ci}) / \pi f$. By inspection, the properties of $h(\pi f \tau_{ci})$ may be summarised as follows (herein only its behaviours for $f \ge 0$ are considered). $h(\pi f \tau_{ci})$ has zero crossings at $f \tau_{ci} = \{f \tau_{ci} \in Z | f \tau_{ci} > 0\}$; $h(\pi f \tau_{ci})$ has a global maximum of one at $f \tau_{ci} = 0$ (or f = 0) (apply L'Hopital's rule); $h(\pi f \tau_{ci})$ has a global minimum of $-\tau_{ci} / \pi$ at $f \tau_{ci} = 3/2$; $\pi |h(\pi f \tau_{ci})|$ is modulated by $1/\pi f$; $h(\pi f \tau_{ci})$ has the Taylor series expansion.

Using the last result, it can be shown that $h(\pi f \tau_{ci})$ is approximately a constant next to the origin:

$$h(\pi f\tau_{ci}) \approx 1 - \frac{(\pi f\tau_{ci})^2}{3!} = 1$$
 for $f\tau_{ci} \to 0$ (I.20)

The conclusion from the above properties shows that the contribution to the PSD by a single chord time τ_{ci} is approximately a constant for $f\tau_{ci} \rightarrow 0$, and decays with $1/f^2$ for $f\tau_{ci} \rightarrow \infty$.

With these in mind, the dependence of $E(S_i(f))$ on τ_{ci} is summarised as follows. For $\tau_{ci} \approx 0$, $f\tau_{ci} \approx 0$ for all f; therefore a small chord time contributes approximately equally to all frequency components on the PSD curve. For $\tau_{ci} \gg 0$, $f\tau_{ci} \gg 0$ for all f; thus a large chord time contributes dominantly to the low frequency range of the PSD curve and decays rapidly with $1/f^2$. For intermediate cases the effects are in between.

As a result, the high frequency range of the PSD curve reflects contributions of small chord times, while the low frequency range contains contributions of both small and large chord times.

Using the same methodology, the interactions between each pair of gas/liquid chord times may be studied by analysing the term:

$$g(\pi f \tau_{ci}) = \sin(\pi f \tau_{ci}) \sin(\pi f \tau_{ci}) / (\pi f)^2$$
(I.21)

The Taylor series approximation of Equation (I.21) at the origin up to the second order is:

$$g(\pi f\tau_{ci}) \approx \left(1 - \frac{(\pi f\tau_{ci})^2}{3!}\right) \left(1 - \frac{(\pi f\tau_{cj})^2}{3!}\right) \qquad \text{for } f\tau_{ci} \to 0 \text{ (I.22)}$$

By inspection of Equation (I.22), the interactions between the smallest bubbles contribute approximately uniformly to the entire frequency range of the spectrum $(g(\pi f \tau_{ci}) \approx 1)$, while any interactions involving large bubbles will have an effect that decays with $1/f^2$.

References and bibliography

- Bertola, N.J., Wang, H., and Chanson, H. (2018), "Air Bubble Entrainment, Breakup and Interplay in Vertical Plunging Jets." *Journal of Fluids Engineering*, ASME, Vol. 140, No. 9, Paper 091301, 13 pages (DOI: 10.1115/1.4039715).
- Cain, P., and Wood, I.R. (1981). "Measurements of Self-aerated Flow on a Spillway." Jl. Hyd. Div., ASCE, 107, HY11, pp. 1425-1444.
- Cartellier, A., and Achard, J.L. (1991). "Local Phase Detection Probes in Fluid/Fluid Two-Phase Flows." *Rev. Sci. Instrum.*, Vol. 62, No. 2, pp. 279-303.
- Chanson, H. (1997). "Air Bubble Entrainment in Free-Surface Turbulent Shear Flows." Academic Press, London, UK, 401 pages.
- Chanson, H. (2002). "Air-Water Flow Measurements with Intrusive Phase-Detection Probes. Can we Improve their Interpretation ?" *Journal of Hydraulic Engineering*, ASCE, Vol. 128, No. 3, pp. 252-255 (DOI: 10.1061/(ASCE)0733-9429(2002)128:3(252)).
- Chanson, H. (2016). "Phase-Detection Measurements in Free-Surface Turbulent Shear Flows." *Journal of Geophysics and Engineering*, Vol. 13, No. 2, pp. S74-S87 (DOI: 10.1088/1742-2132/13/2/S74).
- Chanson, H., and Gonzalez, C.A. (2004). "Interactions between Free-surface, Free-stream Turbulence and Cavity Recirculation in Open Channel Flows: Measurements and Turbulence Manipulation." *Proceedings* 5th International Conference on Multiphase Flow, Yokohama, Japan, Y. Matsumoto, K. Hishida, A. Tomiyama, K. Mishima and S. Hosokawa editors, Paper 104, 14 pages.
- Crowe, C., Sommerfield, M., and Tsuji, Y. (1998). "Multiphase Flows with Droplets and Particles." *CRC Press*, Boca Raton, USA, 471 pages.
- Ervine, D.A., McKeogh, E.J., and, Elsawy, E.M. (1980). "Effect of Turbulence Intensity on the rate of Air Entrainment by Plunging Water Jets." *Proc. Instn Civ. Engrs*, Part 2, June, pp. 425-445.
- Felder, S., and Chanson, H. (2016). "Air-water flow characteristics in high-velocity free-surface flows with 50% void fraction." *International Journal of Multiphase Flow*, Vol. 85, pp. 186-195(DOI: 10.1016/j.ijmultiphaseflow.2016.06.004).
- Gnedenko, B.V., and Kolmogorov, A.N. (1949). "Limiting distributions for sums of independent random quantities." *Gostekhizdat*, Moscow.
- Gonzalez, C.A. (2005). "An Experimental Study of Free-Surface Aeration on Embankment Stepped Chutes." *Ph.D. thesis*, Department of Civil Engineering, The University of Queensland, Brisbane, Australia.
- Hoyt, J.W., and Taylor, J.J. (1977). "Turbulence Structure in a Water Jet Discharging in Air." *Physics of Fluids*, Vol. 20, No. 10, Pt. II, Oct., pp. S253-S257.
- Jones, O.C., and Delhaye, J.M. (1976). "Transient and Statistical Measurement Techniques for two-Phase Flows: a Critical Review." *International Journal of Multiphase Flow*, Vol. 3, pp. 89-116.
- Mirai, Y., Oishi, Y., Takeda, Y., and Yamamoto, F. (2006). "Turbulent Shear Stress Profiles in a Bubbly Channel Flow Assessed by Particle Tracking Velocimetry." *Experiments in Fluids*, Vol. 41, pp. 343-352.
- Oppenheim, A.V., and Schafer, R.W. (2010). "Discrete-time signal processing." *Pearson*, Upper Saddle River N.J., 3rd edition, 1108 pages.
- Papoulis, A., and Pillai, S.U. (2002). "Probability, random variables, and stochastic processes." *McGraw-Hill*, Boston, 4th edition, 852 pages.
- Press, W.H., Flannery, B.P., Teukolsky, S.A., and Vetterling, W.T. (1986). "Numerical recipes: the art of

scientific computation." *Cambridge University Press*, Cambridge Cambridgeshire; New York, 818 pages. Rao, N.S.L., and Kobus, H.E. (1971). "Characteristics of Self-Aerated Free-Surface Flows." *Water and Waste Water/Current Research and Practice*, Vol. 10, Eric Schmidt Verlag, Berlin, Germany.

- Toombes, L., and Chanson, H. (2008). "Interfacial Aeration and Bubble Count Rate Distributions in a Supercritical Flow Past a Backward-Facing Step." *International Journal of Multiphase Flow*, Vol. 34, No. 5, pp. 427-436 (doi.org/10.1016/j.ijmultiphaseflow.2008.01.005).
- Welch, P. (1967). "The use of fast fourier transform for the estimation of power spectra: A method based on time averaging over short, modified periodograms." *IEEE Transactions on Audio and Electroacoustics*, Vol. 15, No. 2, pp. 70-73. (DOI:10.1109/TAU.1967.1161901).
- Wood, I.R. (1991). "Air Entrainment in Free-Surface Flows." *IAHR Hydraulic Structures Design Manual* No. 4, Hydraulic Design Considerations, Balkema Publ., Rotterdam, The Netherlands, 149 pages.
- Zhang, G., and Chanson, H. (2016). "Interactions between Free-surface Aeration and Total Pressure on a Stepped Chute." *Experimental Thermal and Fluid Science*, Vol. 74, pp. 368-381 (DOI: 10.1016/j.expthermflusci.2015.12.011)
- Zhang, G., and Chanson, H. (2017). "Self-aeration in the rapidly- and gradually-varying flow regions of steep smooth and stepped spillways." *Environmental Fluid Mechanics*, Vol. 17, No. 1, pp. 27-46 (DOI: 10.1007/s10652-015-9442-z).