

- (b) Using the momentum integral equation, calculate the boundary shear stress at  $x = 0.1$  m.
- (c) Based upon the momentum integral equation, integrate numerically the boundary shear stress to estimate the friction force per unit width on the 0.2 m long plate.
- (d) Compare your results with the theoretical calculations (Blasius equation) and with the approximate solution assuming a quadratic velocity distribution. *Check that the flow laminar before conducting the comparison.*

The fluid is a bentonite suspension (density:  $1115 \text{ kg/m}^3$ , viscosity:  $0.19 \text{ Pa}\cdot\text{s}$ , mass concentration: 17%).

*Solution*

- (a) The free-stream velocity is about 11.6 cm/s.

(b)

	Momentum integral equation	Blasius solution
$\tau_o (x=0.1 \text{ m}) (\text{Pa}) =$	0.41	0.6
$F_{\text{shear}}/B (\text{N/m}) =$	0.083 (?)	0.17

Note: The application of the momentum integral equation between  $x = 0$  and  $x = 0.05$  m not impossible, but this region is affected by large shear stress because of the flow singularity.

### **EXERCISE NO. 5**

Assuming that the velocity profile in a laminar boundary layer satisfies a polynomial of fourth degree, apply the momentum integral equation.

- (a) Derive the expression of the velocity profile. *Write carefully the boundary conditions.*
- (b) Derive mathematically the expression of the boundary layer thickness, bed shear stress and total shear force.

### **EXERCISE NO. 6**

Assuming that the velocity profile in a laminar boundary layer satisfies a polynomial of third degree, apply the momentum integral equation.

- (a) Derive the expression of the velocity profile. *Write carefully the boundary conditions.*
- (b) Derive mathematically the expression of the boundary layer thickness, displacement thickness and momentum thickness.
- (c) Derive the expressions of the bed shear stress and total shear force.
- (d) Compare your results with the Blasius solution.

*Solution*

- (a) Let us assume that the velocity profile above a flat plate may be expressed as :

$$\frac{V_x}{V_o} = a_0 + a_1 \times \frac{y}{\delta} + a_2 \times \left(\frac{y}{\delta}\right)^2 + a_3 \times \left(\frac{y}{\delta}\right)^3$$

where  $a_0, a_1, a_2$  and  $a_3$  are undetermined coefficients, The coefficients are determined from the boundary conditions :  $v_x(y=0) = 0, v_x(y=+\infty) = V_o, (\partial v_x/\partial y) = 0$  for  $y = \delta$  and  $(\partial^2 v_x/\partial y^2) = 0$  for  $y = \delta$  The velocity distribution is found to be:

$$\frac{v_x}{V_o} = 3 \times \frac{y}{\delta} - 3 \times \left(\frac{y}{\delta}\right)^2 + \left(\frac{y}{\delta}\right)^3$$

(b) The von Karman momentum integral equation for a flat plate becomes :

$$V_o^2 \times \frac{\partial}{\partial x}(\delta_2) = \frac{\tau_o}{\rho}$$

For a velocity profile satisfying a polynomial of third degree, the momentum thickness equals :

$$\delta_2 = \int_0^{+\infty} \frac{v_x}{V_o} \times \left(1 - \frac{v_x}{V_o}\right) \times dy = \frac{3}{28} \times \delta$$

The bed shear stress is defined as:

$$\tau_o = \mu \times \left(\frac{\partial v_x}{\partial y}\right)_{y=0} = \frac{3 \times \mu \times V_o}{\delta}$$

The momentum integral equation yields :

$$\frac{3}{28} \times V_o^2 \times \frac{\partial \delta}{\partial x} = \frac{\mu}{\rho} \times \frac{3 \times V_o}{\delta}$$

The integration gives the expression of the boundary layer growth:

$$\delta = \sqrt{14} \times \frac{x}{\sqrt{Re_x}}$$

The displacement thickness and momentum thickness equal:

$$\delta_1 = \frac{\delta}{4} = \sqrt{\frac{7}{2}} \times \frac{x}{\sqrt{Re_x}}$$

$$\delta_2 = \frac{3}{28} \times \delta = \sqrt{\frac{9}{56}} \times \frac{x}{\sqrt{Re_x}}$$

(c) The boundary shear stress is deduced from the momentum integral equation:

$$\frac{\tau_o}{\frac{1}{2} \times \rho \times V_o^2} = 2 \times \frac{\partial}{\partial x}(\delta_2) = \sqrt{\frac{9}{56}} \times \frac{1}{\sqrt{Re_x}}$$

The dimensionless boundary shear force per unit width equals:

$$\frac{\int_0^L \tau_o \times dx}{\frac{1}{2} \times \rho \times V_o^2 \times L} = \sqrt{\frac{9}{14}} \times \frac{1}{\sqrt{Re_L}}$$

(d) The results are compare with the Blasius analytical solution below:

Boundary layer parameter	Approximate solution	Theoretical solution
Velocity distribution:	$\frac{v_x}{V_0} = 3 \times \frac{y}{\delta} - 3 \times \left(\frac{y}{\delta}\right)^2 + \left(\frac{y}{\delta}\right)^3$	Blasius equation
$\delta =$	$3.74 \times \frac{x}{\sqrt{Re_x}}$	$4.91 \times \frac{x}{\sqrt{Re_x}}$
$\delta_1 =$	$1.87 \times \frac{x}{\sqrt{Re_x}}$	$1.72 \times \frac{x}{\sqrt{Re_x}}$
$\delta_2 =$	$0.40 \times \frac{x}{\sqrt{Re_x}}$	$0.664 \times \frac{x}{\sqrt{Re_x}}$
$\frac{\tau_0}{\frac{1}{2} \times \rho \times V_0^2}$	$\frac{0.40}{\sqrt{Re_x}}$	$\frac{0.664}{\sqrt{Re_x}}$
$\frac{L \int_{x=0} \tau_0 \times dx}{\frac{1}{2} \times \rho \times V_0^2 \times L}$	$\frac{0.80}{\sqrt{Re_L}}$	$\frac{1.328}{\sqrt{Re_L}}$

### **EXERCISE NO. 7**

Let us consider a laminar wake behind a 0.5 m long plate.

(a) Calculate the total drag force (per unit width) on the plate.

(b) Estimate at what distance, downstream of the plate, the velocity profile will recovers (within 2% of the free-stream velocity) ?

The free-stream velocity is 0.35 m/s and the fluid is a viscous SAE40 oil (density: 871 kg/m<sup>3</sup>, viscosity: 0.6 Pa.s).

*Solution*

(a) Drag per unit width = 4.4 N/m

(b) x/L = 350 (x = 175 m !!!)

### **EXERCISE NO. 8**

Some fluid is injected in a vast container where the surrounding fluid is at rest. The nozzle height is 0.15 mm and the injected velocity is 1 cm/s.

(b) Calculate the maximum jet velocity at distances of 1.5 mm, 2 cm and 18 cm from the nozzle.

(b) At a distance of 18 cm from the nozzle, estimate the volume discharge of entrained fluid (per unit width).

Assume a two-dimensional jet.

The fluid is blood (density: 1050 kg/m<sup>3</sup>, viscosity: 4 E-3 Pa.s).